

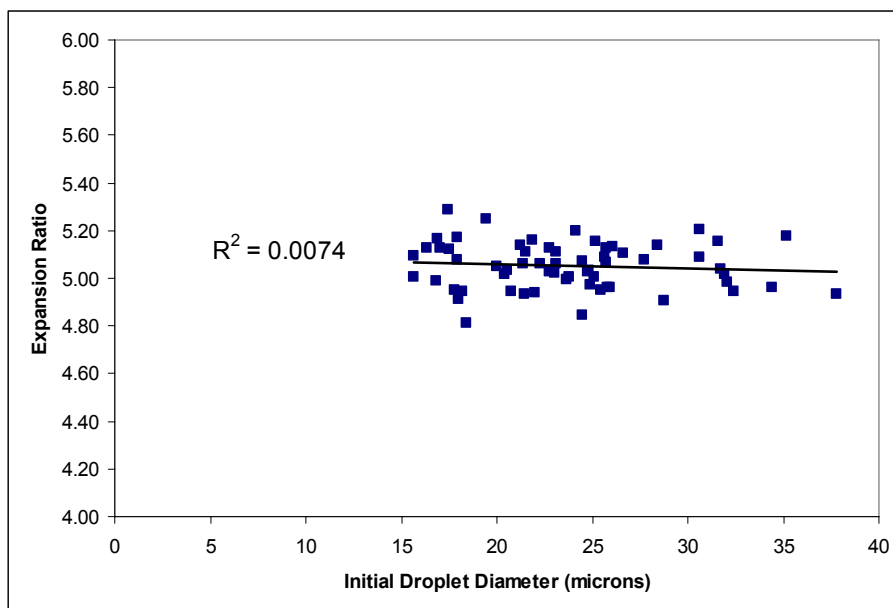
Electronic Supplemental Information for

Bubble Evolution in Acoustic Droplet Vaporization at Physiological Temperature via Ultra-High Speed Imaging

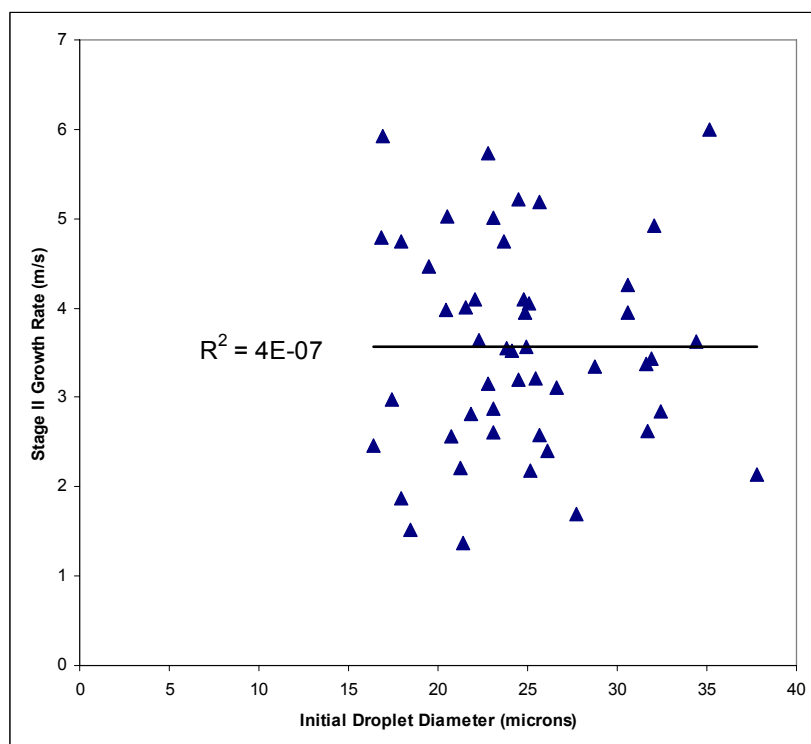
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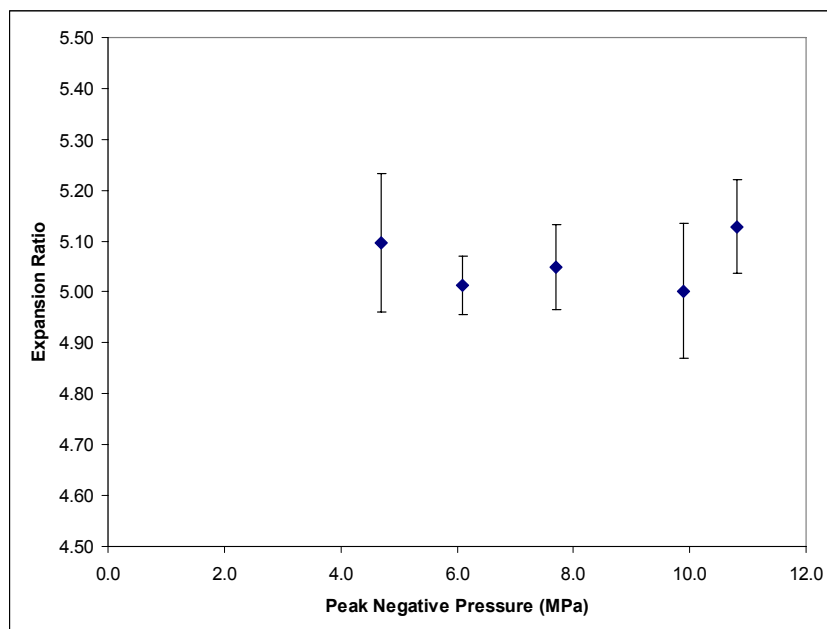
Supplementary Information (deposited electronically on journal website)



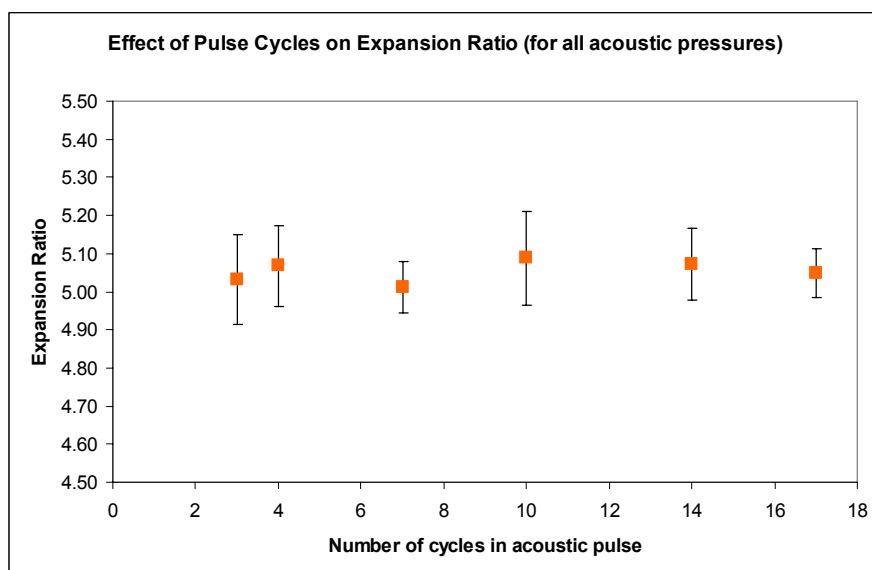
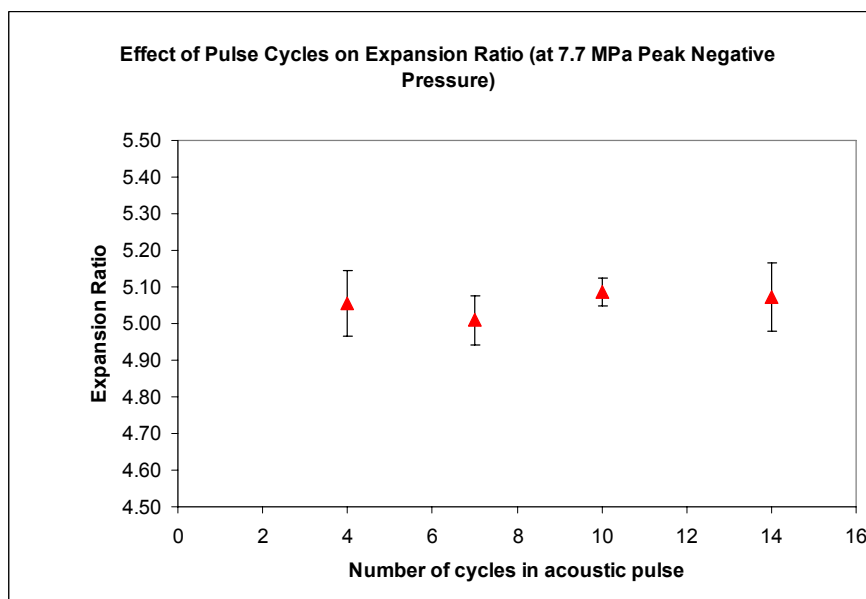
Effect of initial droplet size on the expansion ratio



Effect of initial droplet size on Stage II linear growth rate



Effect of acoustic pressure on expansion ratio



| At 7.7 MPa | | | T-Test p value | | | | | | |
|------------------------|-----------|----------|----------------|-------|-------|-------|-------|-------|--|
| No. Cycles | Exp Ratio | Std Dev | 4 | 7 | 10 | 14 | | | |
| 4 | 5.06 | 0.088444 | NA | 0.180 | 0.437 | 0.762 | | | |
| 7 | 5.01 | 0.067961 | | NA | 0.122 | 0.299 | | | |
| 10 | 5.09 | 0.037594 | | | NA | 0.805 | | | |
| 14 | 5.07 | 0.094202 | | | | NA | | | |
| All acoustic pressures | | | T-Test p value | | | | | | |
| No. Cycles | Exp Ratio | Std Dev | 3 | 4 | 7 | 10 | 14 | 17 | |
| 3 | 5.03 | 0.117652 | NA | 0.573 | 0.730 | 0.467 | 0.597 | 0.808 | |
| 4 | 5.07 | 0.105262 | | NA | 0.047 | 0.708 | 0.924 | 0.649 | |
| 7 | 5.01 | 0.067682 | | | NA | 0.199 | 0.304 | 0.370 | |
| 10 | 5.09 | 0.121375 | | | | NA | 0.823 | 0.525 | |
| 14 | 5.07 | 0.094202 | | | | | NA | 0.696 | |
| 17 | 5.05 | 0.064227 | | | | | | NA | |
| | | | T-Test p value | | | | | | |
| M-Pa | Exp Ratio | Std Dev | 4.7 | 6.1 | 7.7 | 9.9 | 10.8 | | |
| 4.7 | 5.10 | 0.135921 | NA | 0.246 | 0.481 | 0.247 | 0.722 | | |
| 6.1 | 5.01 | 0.057512 | | NA | 0.150 | 0.828 | 0.011 | | |
| 7.7 | 5.05 | 0.08309 | | | NA | 0.361 | 0.055 | | |
| 9.9 | 5.00 | 0.132814 | | | | NA | 0.052 | | |
| 10.8 | 5.12 | 0.086662 | | | | | NA | | |

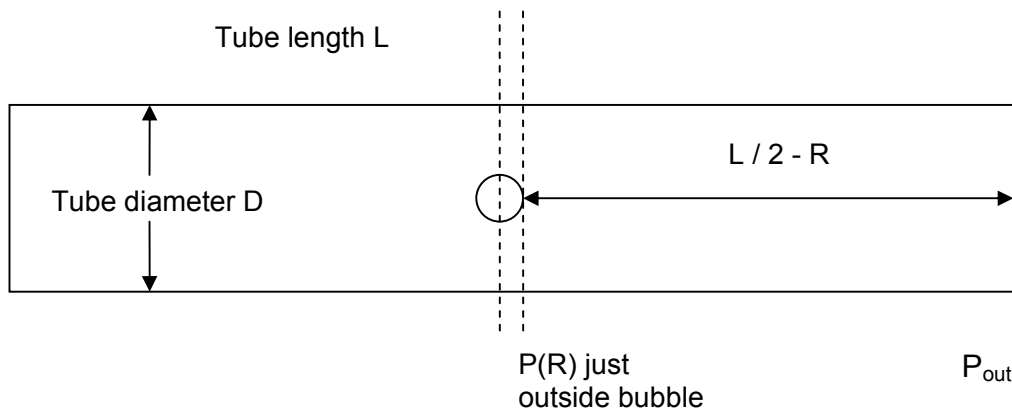
Statistical T-test (two-sided) for Independence of Means

Simplified model of bubble expansion in a tube (details of derivation)

Modified Bernoulli equation (obtain same results if start from conservation of momentum too)

$$\rho \int_{l_1}^{l_2} \frac{\partial \bar{V}}{\partial t} ds + \rho g h_L = P_1 - P_2 \quad (1)$$

P=pressure, \bar{V} = cross-sectional average velocity, s is streamline coordinate, ρ =liquid density, g=acceleration due to gravity, and h_L = head loss



Apply between point ~ at bubble surface to tube outlet, e.g. R to L/2

Assume laminar flow in liquid between bubble and tube outlet to estimate head loss term.

$$\rho g h_L = \frac{64}{\text{Re}} \frac{l}{D} \frac{\rho \bar{V}^2}{2} = \frac{32\mu}{D^2} \left(\frac{L}{2} - R \right) \bar{V} \quad (2)$$

Where D=tube diameter, R=bubble radius, L=tube length.

Conservation of mass for entire tube

$$\frac{d}{dt} \left[\frac{L\pi D^2}{4} - \frac{4\pi R^3}{3} \right] = -\beta Q = -\beta \bar{V} \frac{\pi D^2}{4} \quad (3)$$

where β is the number of outlets (1 or 2)

Rearranging yields

$$\bar{V} = \frac{16}{\beta D^2} R^2 \frac{dR}{dt} \quad (4)$$

$$\frac{d\bar{V}}{dt} = \frac{16}{\beta D^2} \left[R^2 \frac{d^2 R}{dt^2} + 2R \left(\frac{dR}{dt} \right)^2 \right] \quad (5)$$

Pressure jump at the bubble interface (Young-Laplace for moving interface)

$$P(R) = P_{B0} \left(\frac{R_0}{R} \right)^{3\gamma} - \frac{4\mu}{R} \frac{dR}{dt} - \frac{2\sigma}{R} \quad (6)$$

where $P(R)$ is pressure in the liquid at the bubble surface, P_{B0} is initial bubble pressure, $\gamma = 1$ for isothermal expansion (used) or close to 1 for adiabatic expansion of DDFP (1.4 for air), R_0 = initial bubble diameter

Substituting equations (2), (4), (5), and (6) into equation (1) yields

$$\frac{16\rho}{\beta D^2} \left(\frac{L}{2} - R \right) \left[R^2 \frac{d^2 R}{dt^2} + 2R \left(\frac{dR}{dt} \right)^2 \right] + \frac{512\mu}{\beta D^4} \left(\frac{L}{2} - R \right) R^2 \frac{dR}{dt} = P_{B0} \left(\frac{R_0}{R} \right)^{3\gamma} - \frac{4\mu}{R} \frac{dR}{dt} - \frac{2\sigma}{R} - P_{out}$$

Solved with the following parameter values (modifications from these noted in graph):

$\rho = 993.3 \text{ kg/m}^3$
 $\mu = 6 \times 10^{-4} \text{ Ns/m}^2$
 $\sigma = 70 \times 10^{-3} \text{ N/m}$
 $P_{out} = 101300 \text{ Pa}$
 $P_{B0} = 14.6 \times 10^6 \text{ Pa}$

L=16cm

Assumptions:

- Ignores details of flow very close to bubble
- One-dimensional flow model
- Neglect “minor losses”
- Tube length approximation
- Some parameters approximated (e.g. P_{B0} , σ)